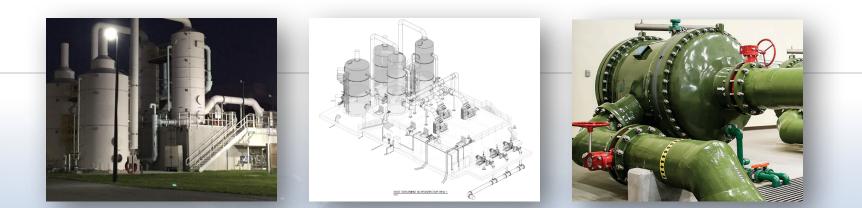
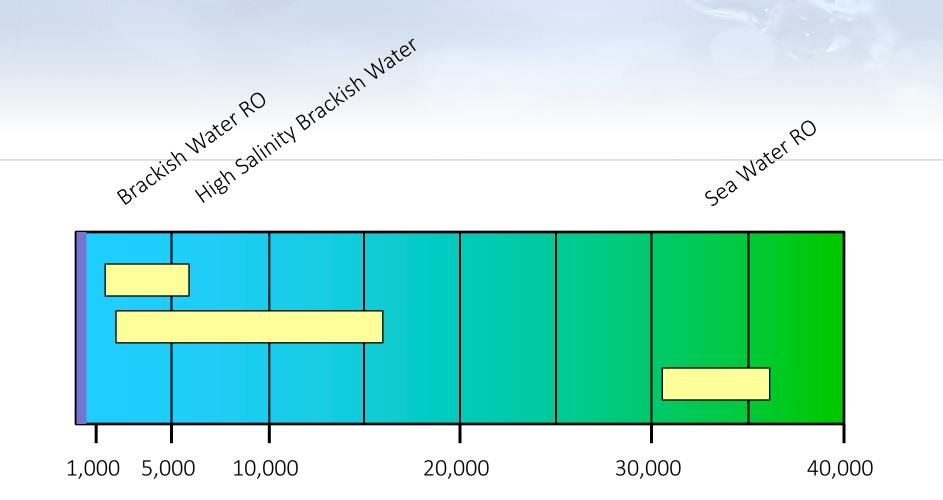
Desalination Process Innovations to Address Extreme Variations in Feed Water Salinity

James E Christopher, PE, BCEE | September 21, 2017



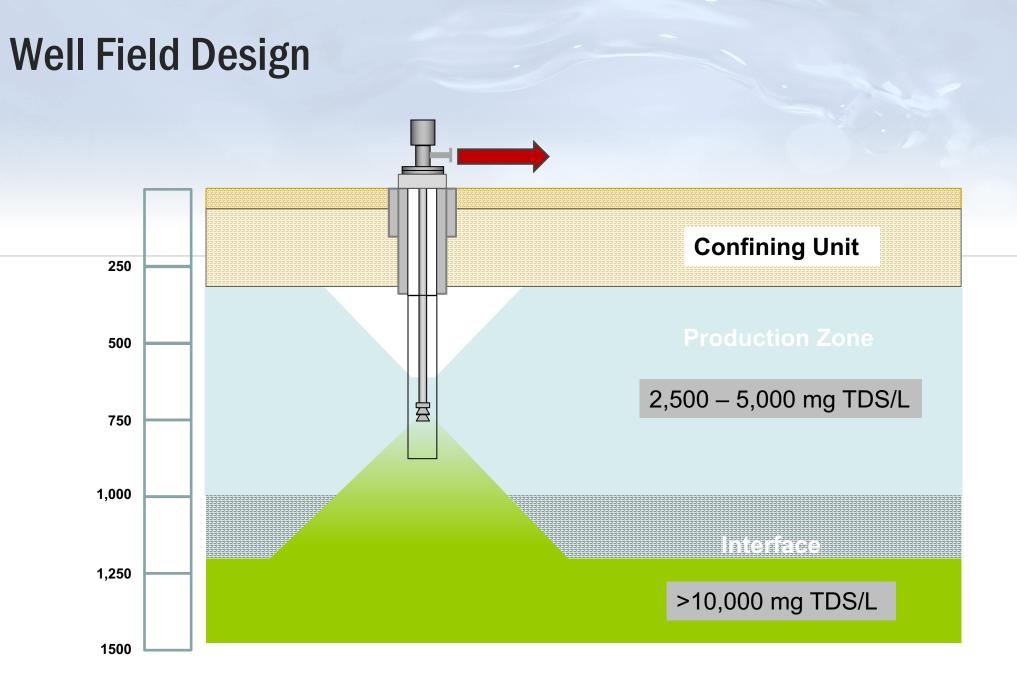


Raw Water Salinity Spectrum



Total Dissolved Solids, mg/L







Raw Water Quality

Parameter	Initial (Year 0)	Well Composite	Degraded (Year 10)
Temperature	23-28 °C	21.8 °C	23-28 °C
TDS, mg/L	1,950	2,602	16,564
рН	7.39 SU	6.2	7.69 SU
Alkalinity, mg/L as CaCO ₃	197	163.3	197
Ca Hardness, mg/L as CaCO ₃	248	340	998
Mg Hardness, mg/L as CaCO ₃	247	436	1,040
Iron, mg/L	0.24	1.13	1.07
Sodium, mg/L	519	708	5,002
Chloride, mg/L	953	1,309	9,067
Sulfate, mg/L	97	183	1,271



Concentrate Disposal

Surface Water Discharge Permit

- Outfall into Anclote Power Plant Cooling Water Discharge Canal
- Copper Limit, 0.0098 mg/L
- Iron Limit, 1.72 mg/L
- Recovery Limited to 65%
- Deep Injection Well
 - Recovery and Quality Not Limited





- Designed for Operation at Initial AND Future Degraded Water Quality
- RO Process Design Criteria
 - Minimum Recovery: 65%
 - Finished Water Capacity: 6.4 MGD
 - Number of RO Trains: Three (3)
 - Membrane Elements: 400 SF/element
 - Average Permeate Flux: ≤ 12 gfd
 - RO Feed Pump Motor: ≤ 800 HP



Finished Water Quality Goals

Parameter	Water Quality Requirements	
pH	≤ 9.0 SU	
Calcium Hardness	\geq 40 mg/L as CaCO ₃	
Alkalinity	≥ 40 mg/L as CaCO ₃	
Iron	0.3 mg/L	
Chloride	250 mg/L	
Sulfate	250 mg/L	
Total Dissolved Solids	500 mg/L	
Langelier Saturation Index (LSI)	0.1-0.5	
Calcium Carbonate Precipitation Potential (CCPP)	4-10 mg/L	
Free Chlorine Residual	0.0-4.0 mg/L as Cl ₂	



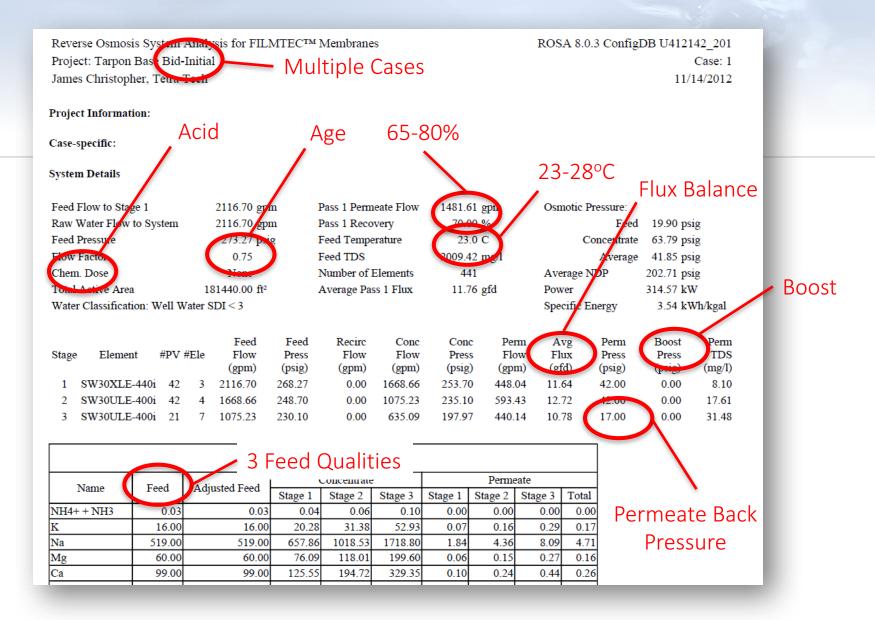
RO System Operational Plan

High rejection seawater RO membranes

- RO membrane flux limits
- High salinity of future degraded raw water
- Designed for variable recovery
 - 75-80% for initial water quality/deep well
 - 65-70% as raw water quality degrades
 - 65% for surface water discharge
- Designed for Variable Permeate Flow Rate



Multiple Membrane Projections



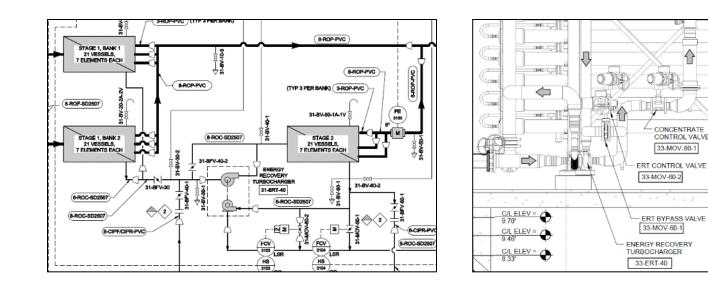
RO Membrane Selection

- 2-Stage, 7-element, 42:21 Array
- 1st Stage hybrid element load, 440 SF and 400 SF elements, to meet 12 gfd flux
- Dow Filmtec SW Membranes
 - 1st Stage Elements 1-3: SW30XLE-440i
 - (99.8% salt rej., 9,900 gpd)
 - 1st Stage Elements 4-7: SW30ULE-400i (99.6% salt rej., 8,400 gpd)
 - 2nd Stage Elements: SW30ULE-400i (99.6% salt rej., 8,400 gpd)



Additional RO Train Features

- Hydraulic Turbocharger for Interstage Boost
 - Greatest boost at degraded raw WQ and 65% system recovery
- Pressure Vessels:
 - Stage 1: 600 psi Rated (max working pressure is 503 psi)
 - Stage 2: 1000 psi Rated (max working pressure is 657 psi)





Materials of Construction

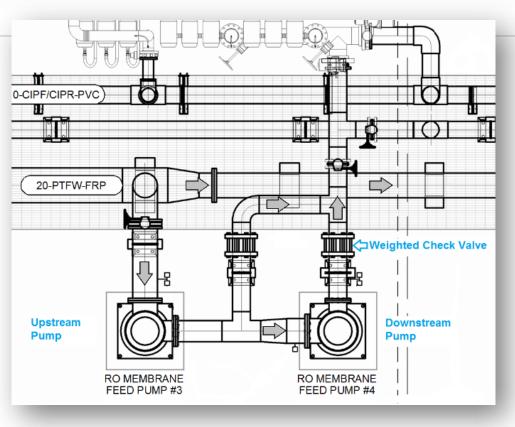
- Raw Water Piping/Pumps
 - Above Grade-Super Duplex SS 2507
 - Below Grade-HDPE, DR 11
- RO Trench Piping/Feed Filters
 - FRP
- RO Feed Pumps/Piping
 - Super Duplex SS 2507, 300/600 lb flanges
- Interstage/Concentrate Piping
 - Super Duplex SS 2507, 600 lb flanges



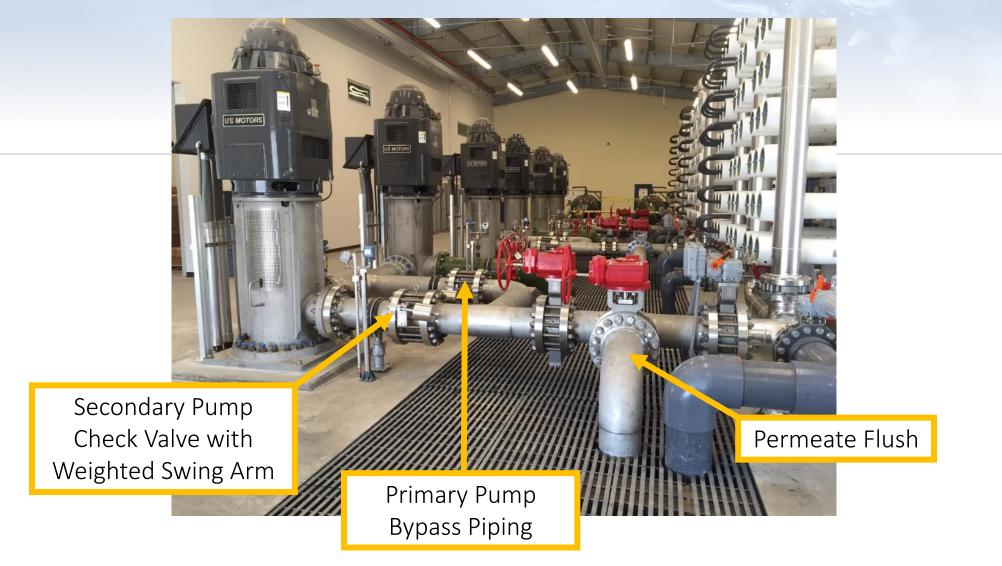


RO Feed Pump Design

- Two feed pumps to satisfy 800 HP limit
- Pumps in series to provide turndown of feed pressure
- One feed pump operates at startup, flow will bypass 2nd pump
- Controls allow operator to select low or high salinity operating mode
- Either pump can be lead

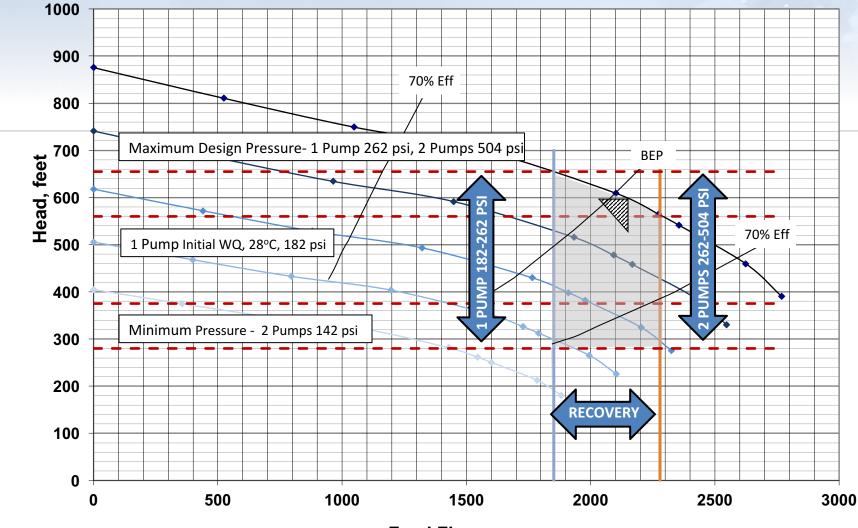


RO Feed Pumps





Feed Pump Operating Envelope

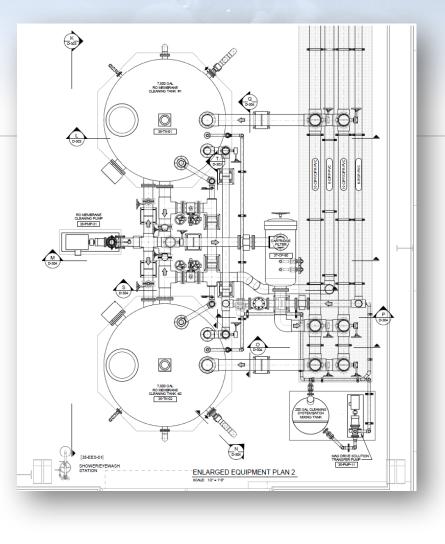


Feed Flow, gpm



RO Process – Permeate Flush System

- Automated Permeate Flush after Shutdown:
 - Upsized CIP tanks to 7,500 gal/each and recirculation pump to 1,000 gpm for dual purposes (CIP/Flush System)
 - Added motorized valve to RO skid's feed pipe
 - Added controls and valves for filling CIP/Flush tanks

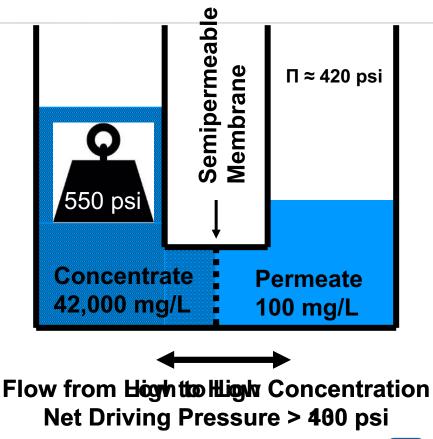




RO Process – Permeate Suck Back

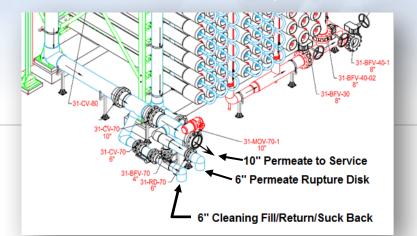
- A sudden loss of feed pressure during operation (Power loss or emergency alarm condition) will lead to a pressure imbalance in the system (RO feed pressure is less than the osmotic pressure)
- As a result, forward osmosis will occur within the membrane elements in a phenomenon known as "permeate suck back"

Osmotoircharegearet Daniven Permeate Suck Back



RO Process – Permeate Suck Back

- Passive "Permeate Suck Back" Provisions: Sized for power loss with 1-2 RO trains in operation
 - Conventional permeate suck back tank not feasible due to static head for degasifiers
 - Permeate stored in the CIP tanks is used the source
 - Cleaning permeate piping to/from RO trains was upsized
 - Additional check and isolation valves installed on RO trains

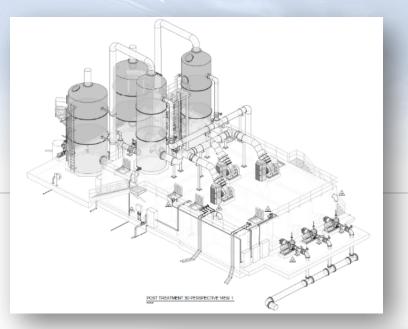






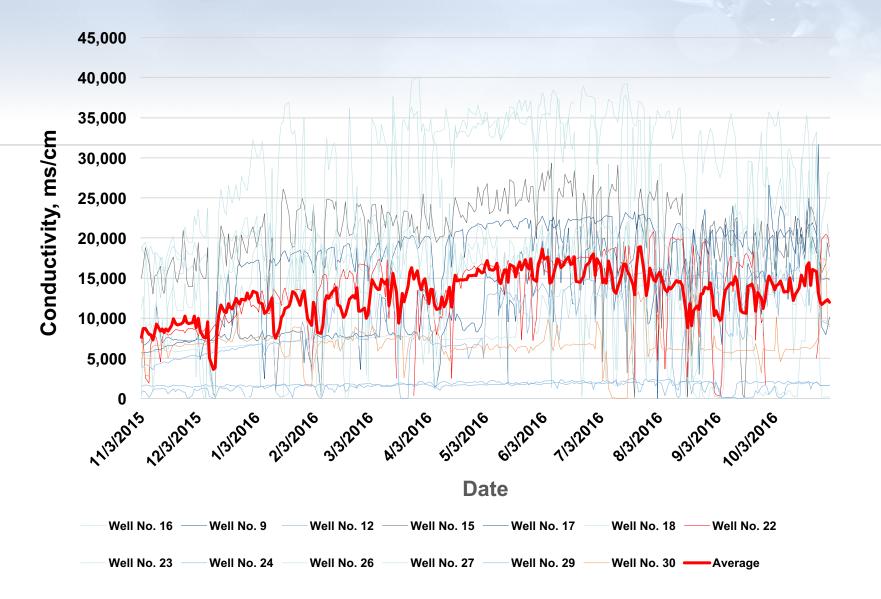
Post Treatment

- Permeate Quality:
 - pH: 5.7
 - Alkalinity: < 2 mg/L as CaCO₃
 - Calcium: < 1 mg/L
- Raw Water Blending
- pH/Ca Adjustment Carbon Dioxide
- Ca/Alkalinity Adjustment, Calcium Hydroxide (Lime) Slurry
- Final pH Adjustment—Sodium Hydroxide



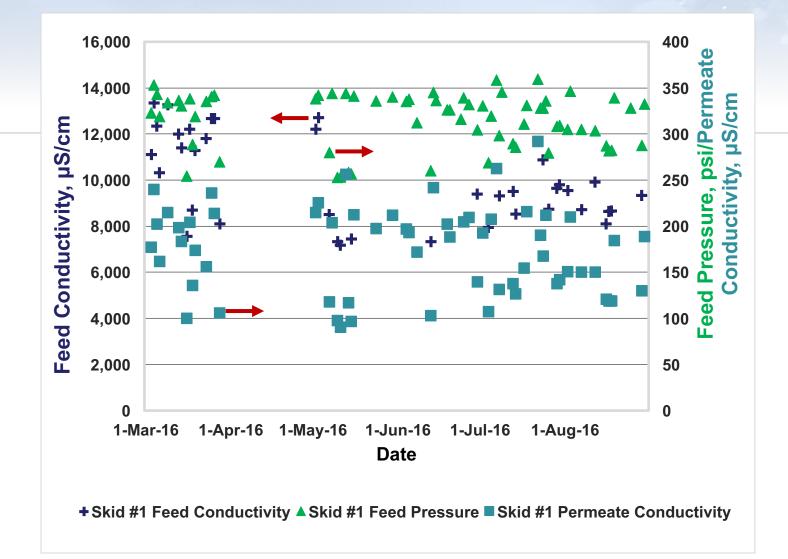


Supply Well Quality





First Year Operating Data







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