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Texas Desal 2018
MANAGING COST, RISK & REGULATION

SEPT 13-14
AUSTIN, TEXAS

**A Case for High Recovery, Low Energy,
Low Cost Desalination with Twin
Turbochargers**

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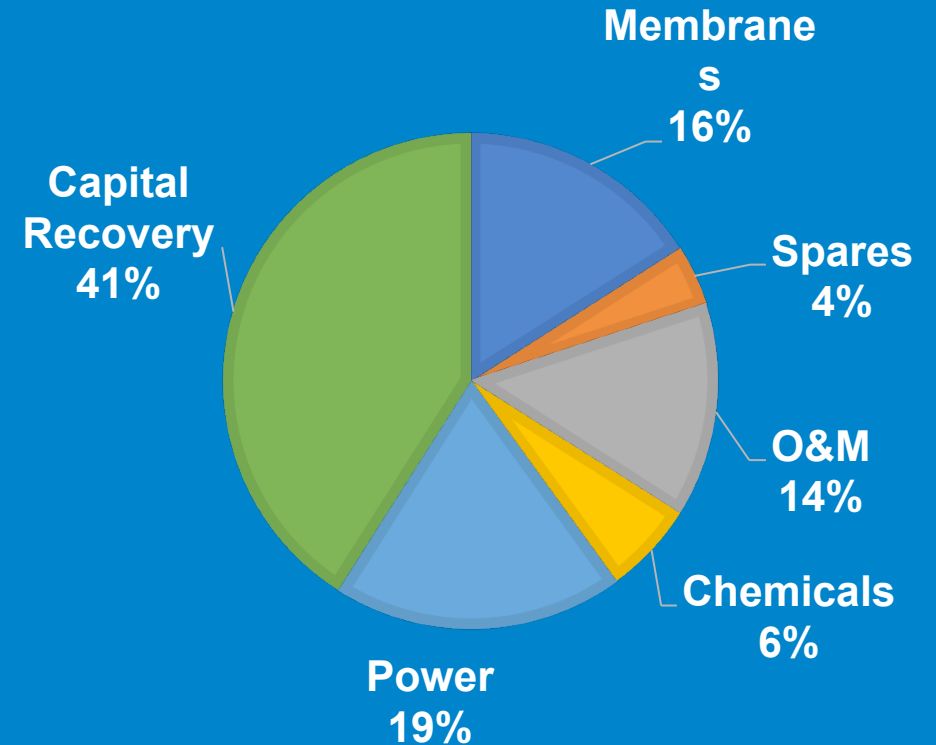
Introduction

- Total Water Cost (TWC)
 - $TWC = CAPEX + OPEX$
 - Does not include distribution costs
- TWC ranges between 0.8 - 2 USD/m³

Cosin C., Desalination Technologies and Economics: CAPEX, OPEX & Technological Game Changers to Come

Ghaffour N. et al., Desalination 309 (2013) 197–207

SEC is less than 20% of Total Cost of Water



Reducing SEC made desal feasible –
how do we make it available?

Applying Known Principles

Today's RO design focuses on only one side of the equation.

$$\text{Horsepower} = \frac{\text{GPM} \times \text{PSI}}{1714 \times \%}$$

Low energy membranes

ERD TRANSFER EFFICIENCY = $\frac{\text{Fluid Power Added to Feed Stream}}{\text{Fluid Power Taken from Brine Stream}}$

Can we use ERDs and other devices to reduce feed GPM and HP?

A kilowatt saved beats 98% of a kilowatt recovered.

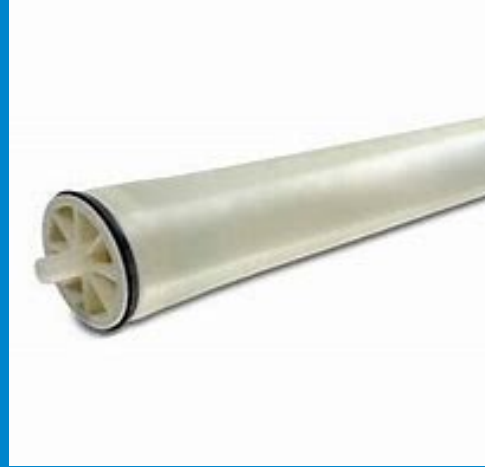
Applying Known Principles

Limitations to increasing recovery?



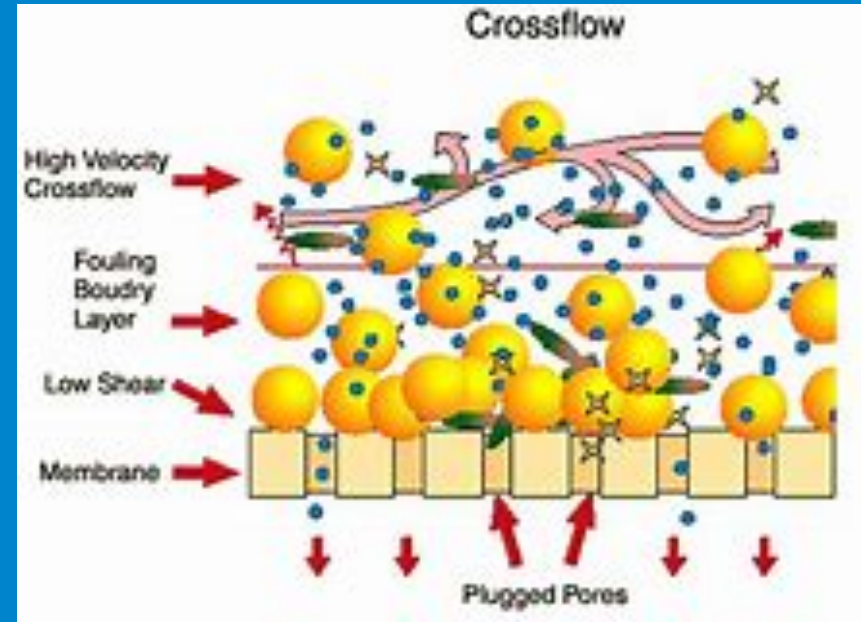
Precipitation

TDS limited by CaCO_3 & CaSO_4 to <90kppm



Pressure

Membranes limited to ~1200 psi (82.7 bar)



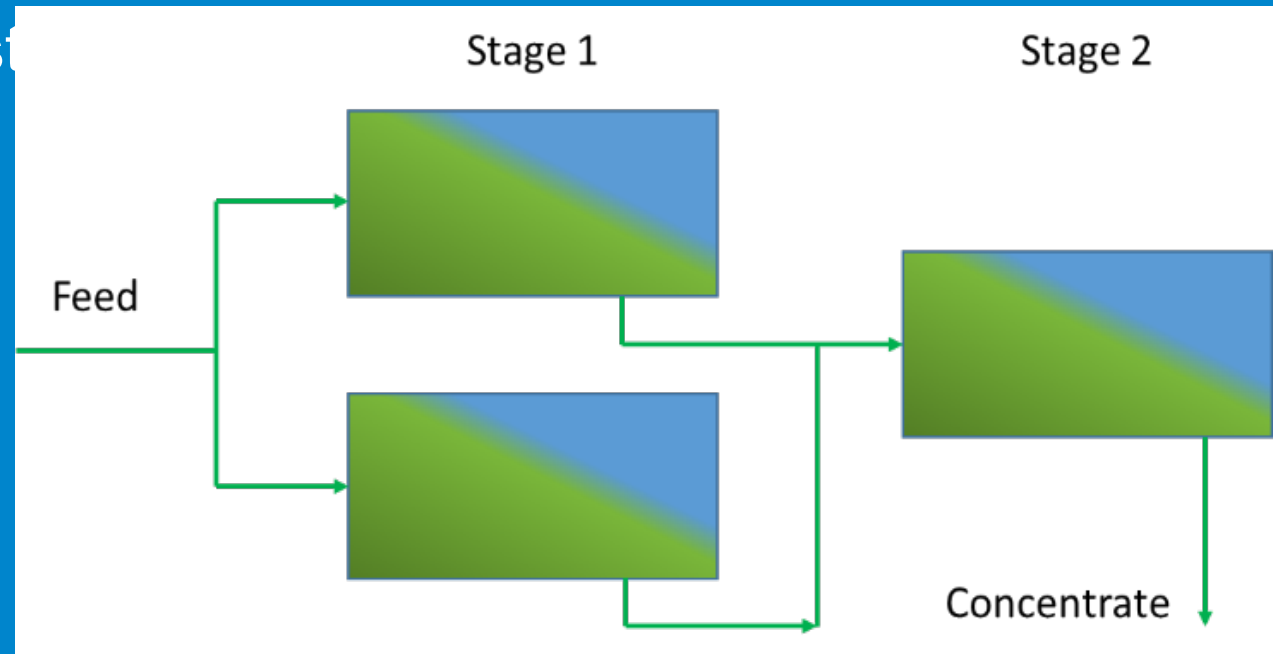
Process

Limits for feed element flux, element recovery, flow velocity

Applying Known Principles

Managing flow *and* pressure is common practice in BWRO systems

- Flow/Velocity Staged RO vessels
- Pressure Interstage boost



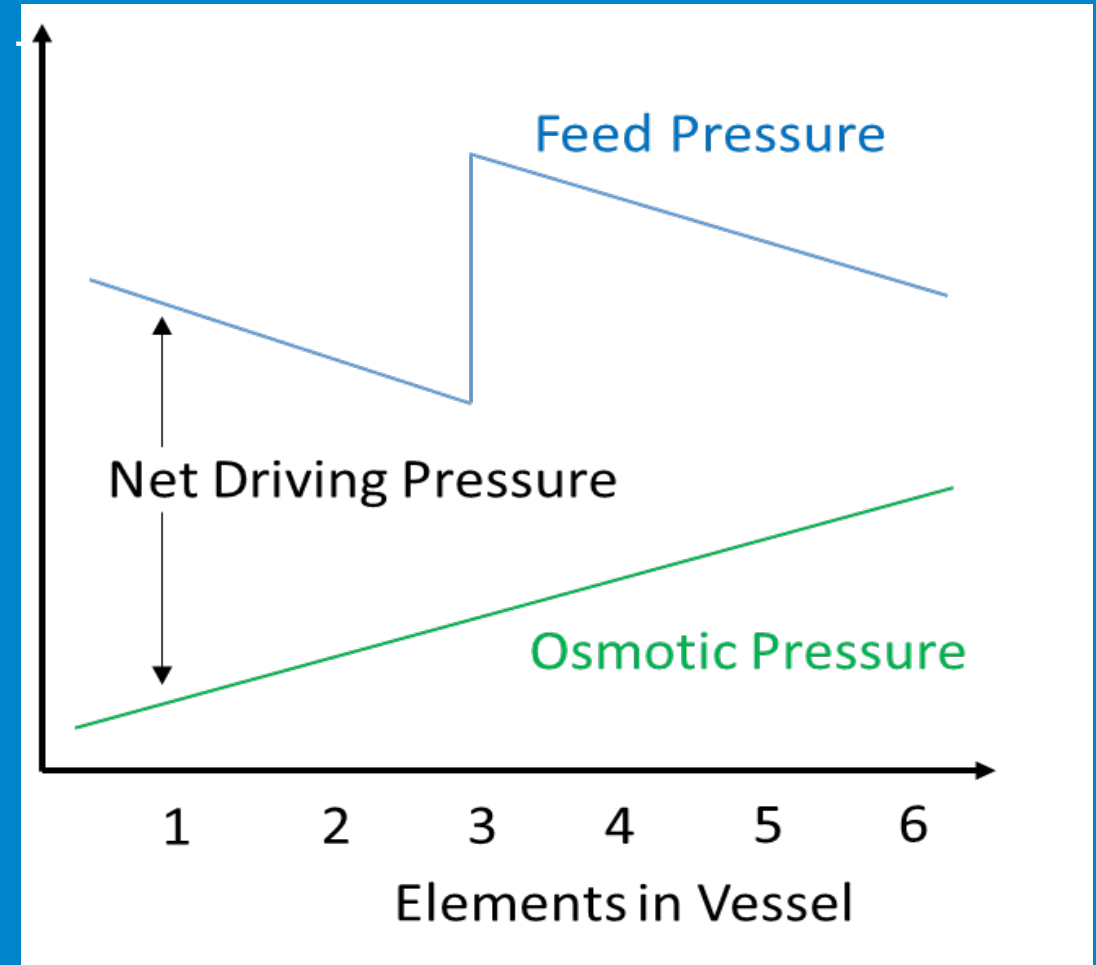
Flux Balancing → Managing Flow & Pressure

Applying Known Principles

Flux Balancing → increased average NDP and

- Manages Net Driving Pressure (NDP)
- Reduces energy consumption
- Improves flow velocity distribution
- Improves pressure distribution
- Distributes fouling → greater resistance
- Lower Beta and scaling potential

Improves membrane
function and life when
applied within
manufacturers' limits



Applying Known Principles

Previous Y2K-era experience with Brine Conversion Systems (BCS)

- Optimum 40%/33% recovery/stage manages salinity rise
- Ten (10) retrofit & newbuild plants
- Toray SU-820BCM

Moch, Jr., I., The Case and feasibility of very high recovery Sea Water Reverse Osmosis Plants, Proceedings, ADA North American Biennial Conference & Exposition, South Lake Tahoe, NV, August 2000

Plant	Recovery	Capacity m ³ /d
Ehime, Japan	60 %	210
Mas Palomas Spain	60 %	270
Ibiza, Spain	60 %	270
Mas Palomas 1 Spain	60 %	4500
KAE Curacao 1 Caribbean	57 %	5700
KAE Curacao 2 Caribbean	57 %	5700
Mas Palomas 2 Spain	60 %	4500
Mas Palomas 3 Spain	60 %	4500
Tortola Caribbean	60 %	690
Muroto Japan	60 %	480

Flux Balancing → Managing Flow & Pressure

Application of Flux Balancing



Turbocharging

- Robust, reliable
- Low CAPEX
- Ease of maintenance



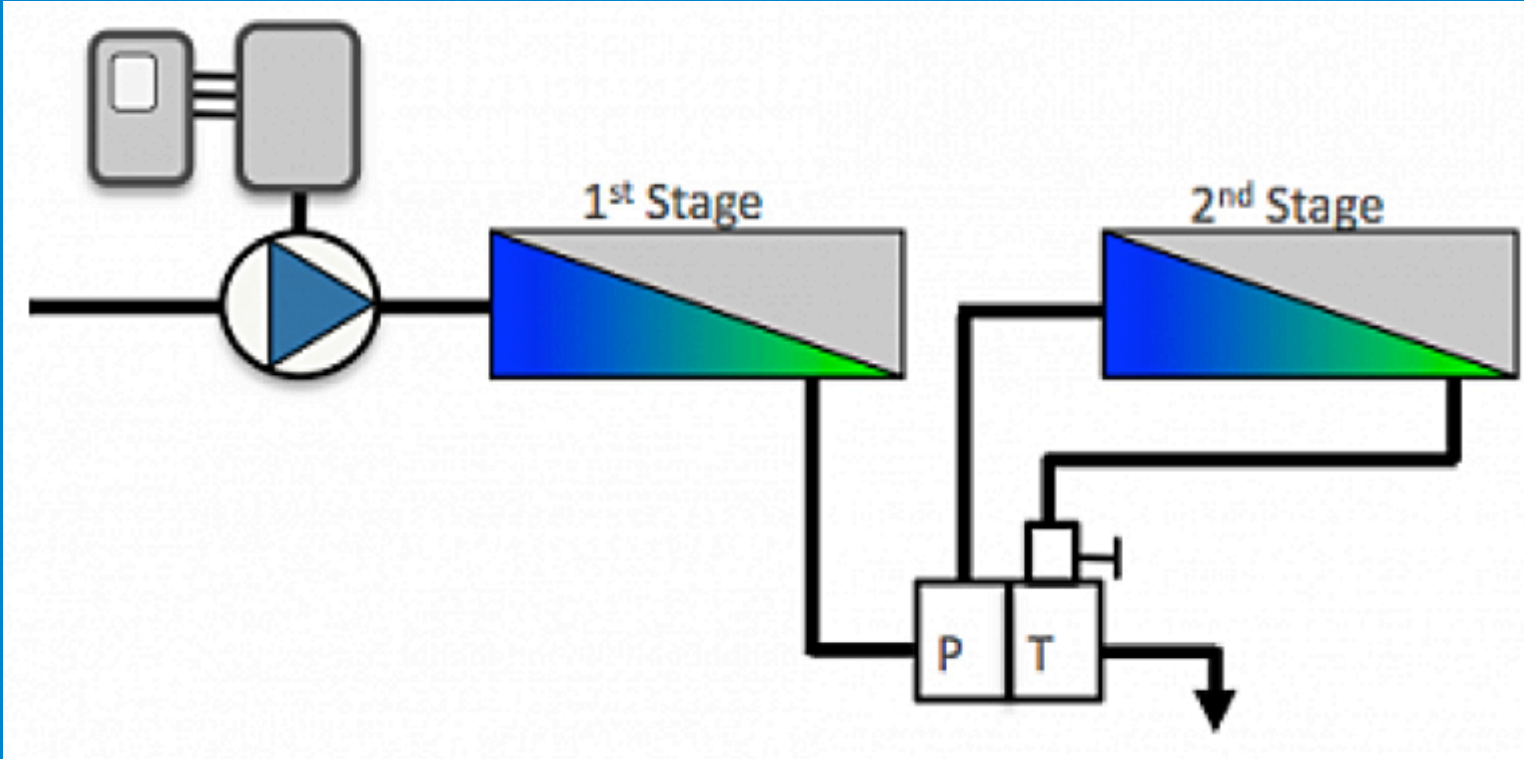
Center Port Vessels

- Managing flow and velocity
- Packaging efficiency

High Recovery SWRO with today's ERD's & pressure vessels

Application of Flux Balancing

Simple Interstage Turbo Booster Arrangement



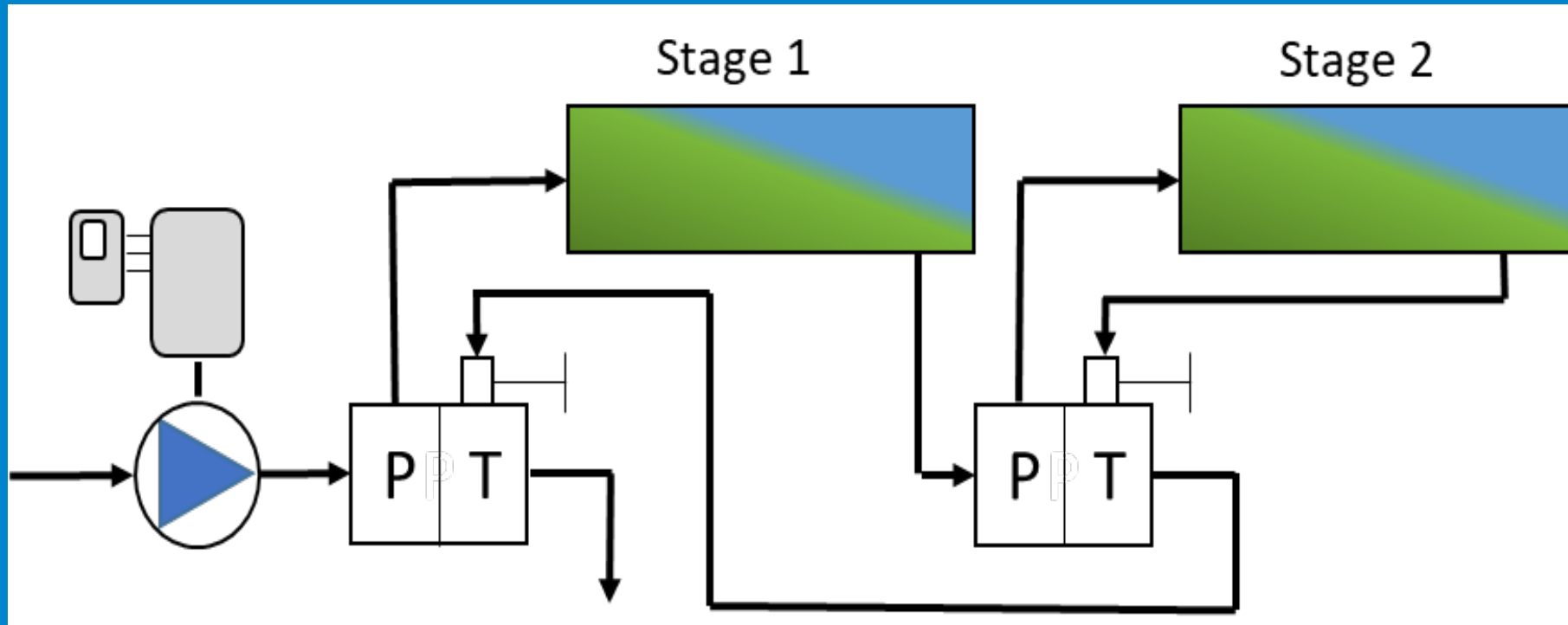
- Simple, robust design
- No additional components
- Ideal for small systems
- Low CAPEX

Flux Balancing → Managing Flow & Pressure

Application of Flux Balancing

Multi Stage / Dual Turbo (MSDT) Arrangement

- Efficient use of brine energy
- Reduce energy consumption
- Flexible flow and flux



Flux Balancing → Managing Flow & Pressure

Effect on Total Cost

Energy and amortization account for 60% of the Total Cost of Water

- Energy cost
 - Directly related to system flux and recovery
- Capital cost
 - Directly related to system flux and recovery
 - Amplified by maintenance and long-term borrowing costs

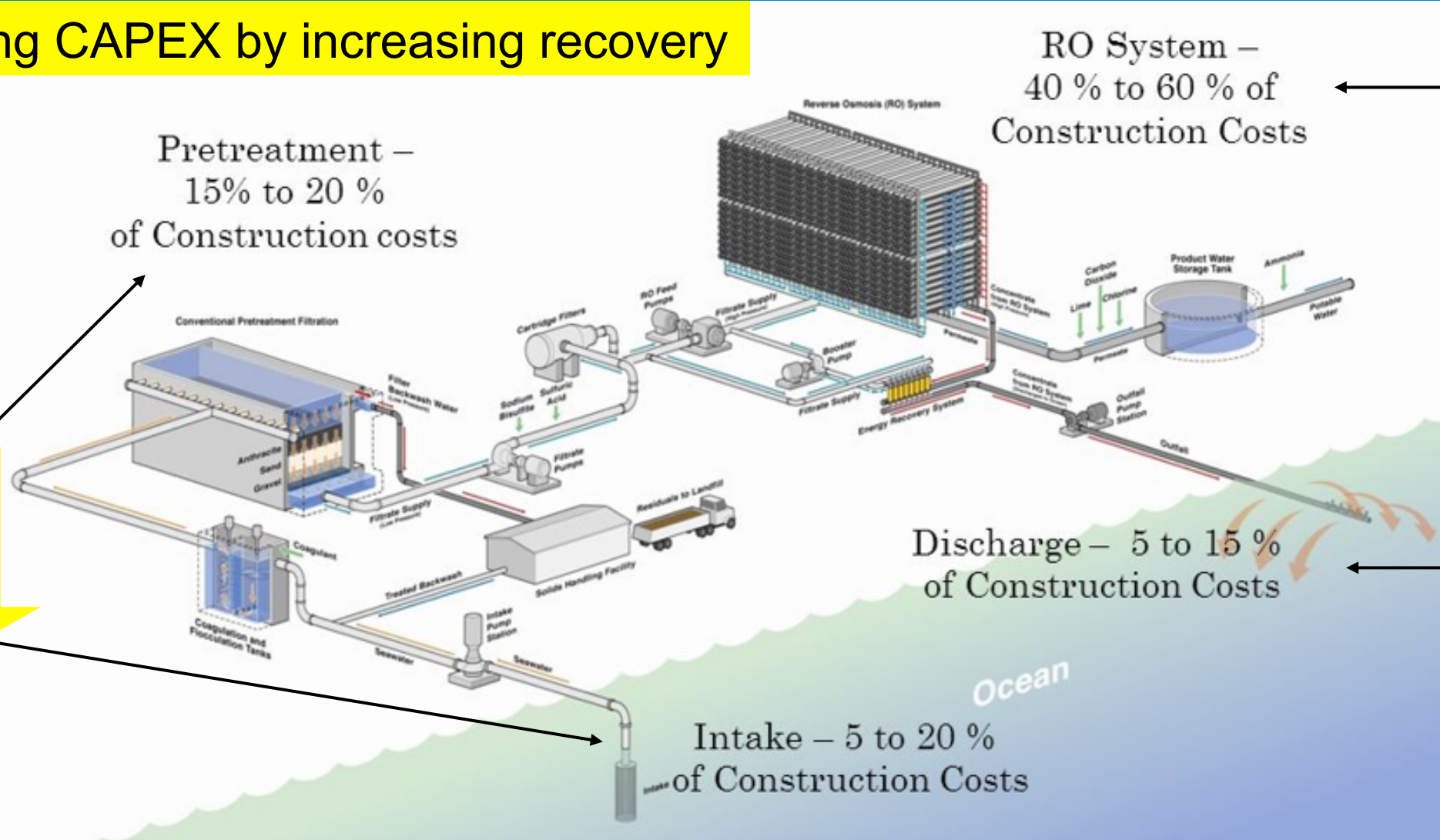
Ghaffour N. et al., Desalination 309 (2013) 197–207

Flux balancing with MSDT reduces Total Cost by increasing recovery

Flux Balancing → Managing Flow & Pressure

Effect on Total Cost

Reducing CAPEX by increasing recovery



600#
First
Stage
?

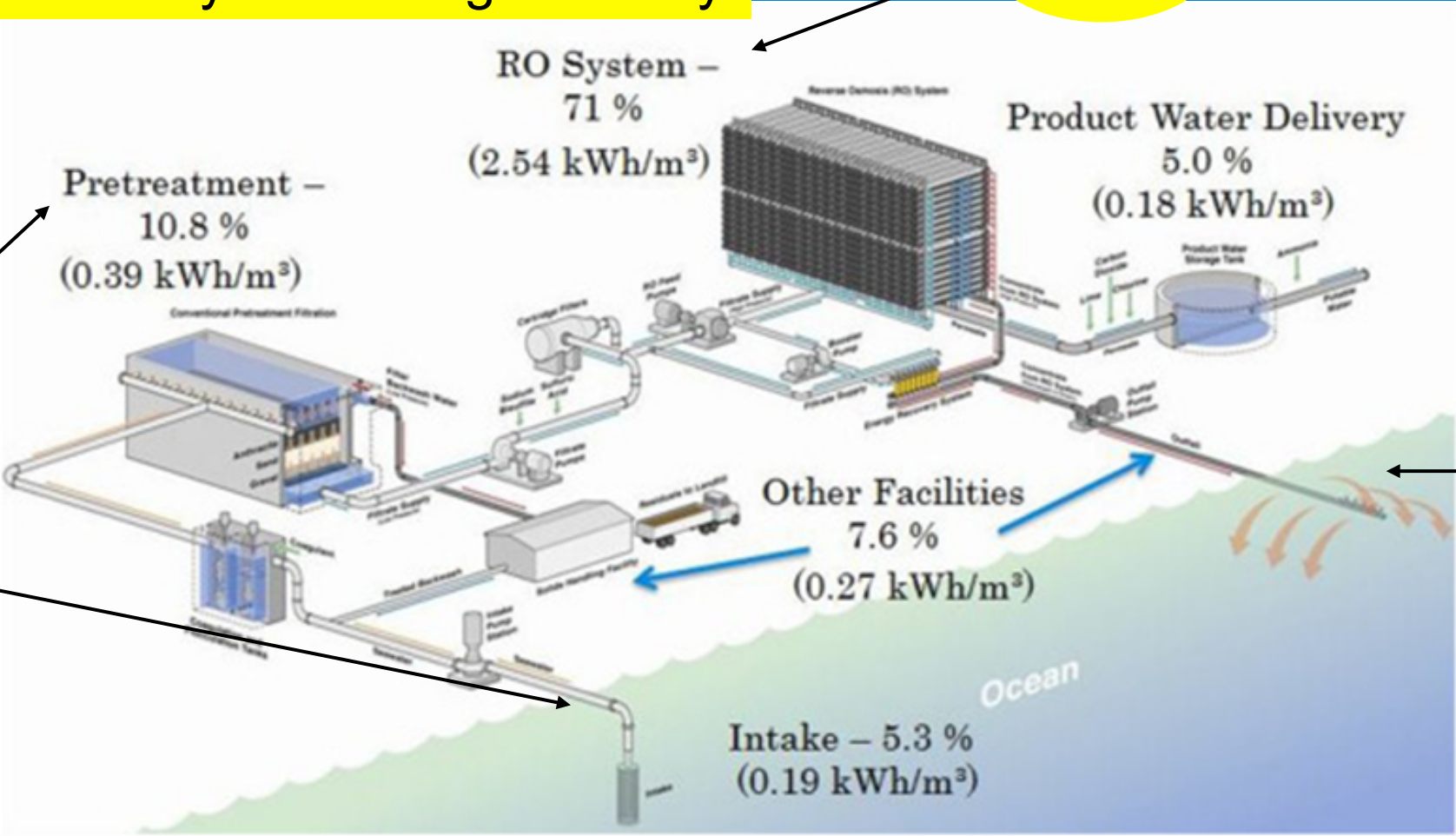
25%

50%

Effect on Total Cost

Reducing Total Cost by increasing recovery

Best SEC



Effect on Total Cost

Case Study	Expected savings
FEDCO	10 - 20 %
Irving Moch, ADA Conference (2000)	10 - 20 %
Meyer- Steele S., et al., Suez, TP1029EN	16%

%	1 Stage	2 Stage
Capital Cost	46%	37%
Electricity	36%	30%
Membrane Replacement	5%	6%
Chemicals	4%	2.5%
Other	9%	8.5%
(Labor, maintenance, etc.)		
Savings	—	16%

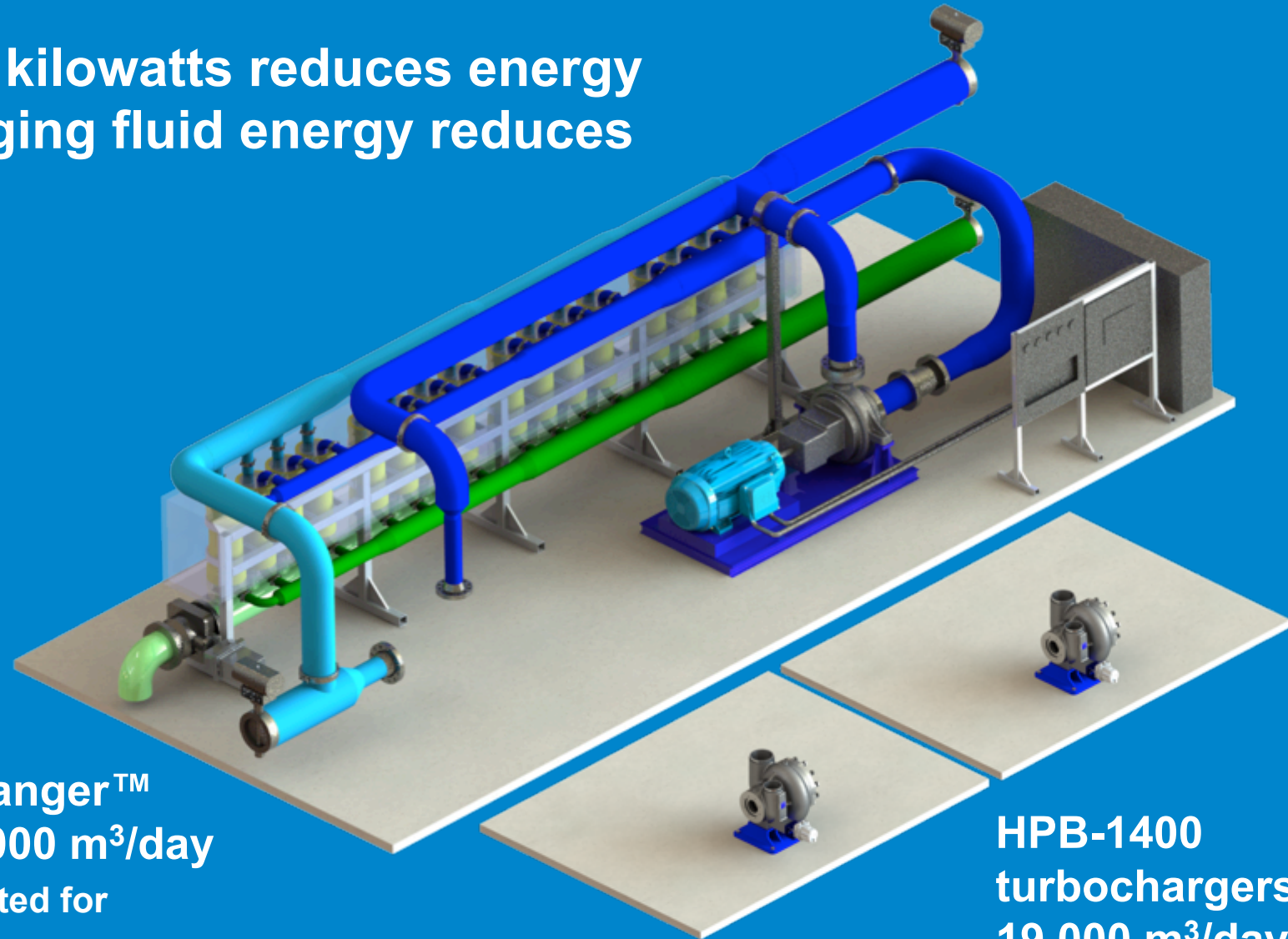
Meyer-Steele S. et al., Seawater reverse osmosis plants in the Caribbean recover energy and brine reduce costs (SUEZ - Technical Paper TP1029EN)

Moch, Jr., I., The Case and feasibility of very high recovery Sea Water Reverse Osmosis Plants, Proceedings, ADA North American Biennial Conference & Exposition, South Lake Tahoe, NV, August 2000

Whether it's CAPEX or OPEX,
a penny saved is still a penny earned.



Transferring kilowatts reduces energy cost. Managing fluid energy reduces everything.



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System for 19,000 m³/day
train (details omitted for
clarity)**

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